

Towards a sustainable fine chemical and pharmaceutical industry: screening and re-utilization of carbon-rich liquid wastes

SH7/2/14



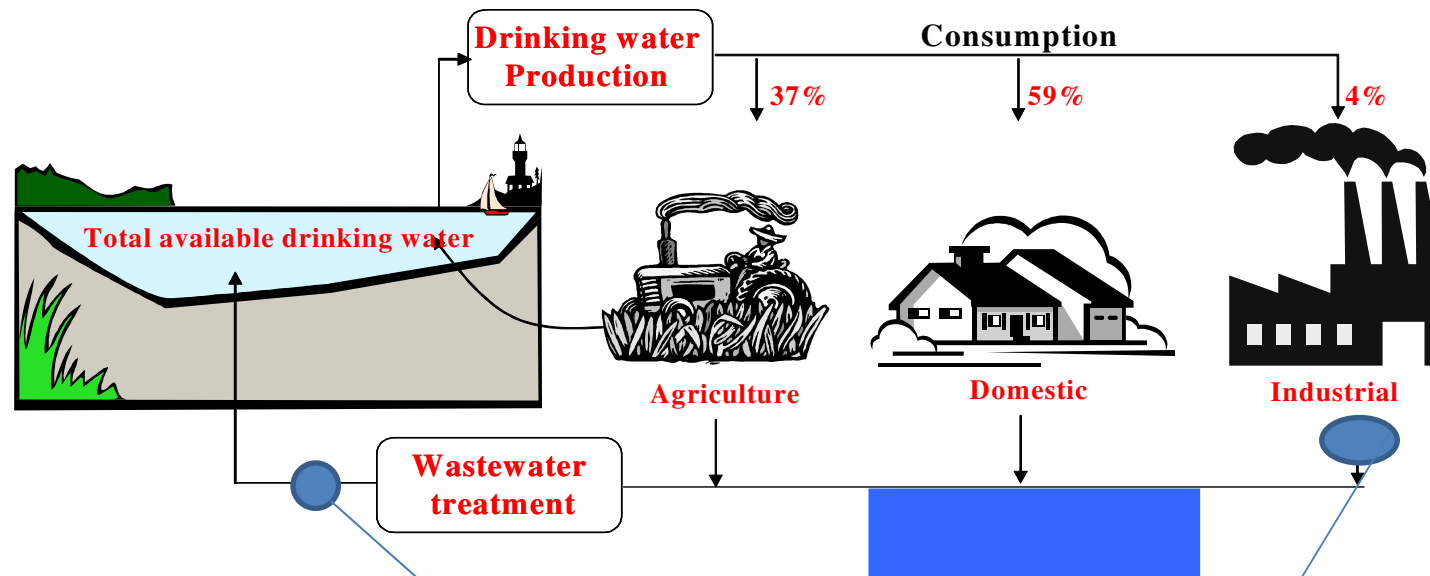
HAS CER (former IOI), BME, BSW, GEOSAN and EPFL

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Content of the presentation

- Introduction of the problem, previous project activities of consortium members
- Starting points of the project
- Testing and treatment methods
- Results in Biodegradation, VOC removal, Wet oxidation, Anaerobic digestion, High energy irradiation+oxidation, AOP processes
- Summary about „half-time” results

Water Cycle in the Center of Human Activities



Emergent organic contaminants (EOCs) are naturally or synthetic substances which:

- have the potential of entering the environment
- cause adverse ecological or negative effects on human health
- most of them are not regulated

Principal *sources* of EOCs are:

- wastewater treatment plants that treat domestic sewage
- wastewater from hospital effluents
- chemical manufacturing plants
- livestock and agriculture

Our activities in these sites



Previous activities of consortium members

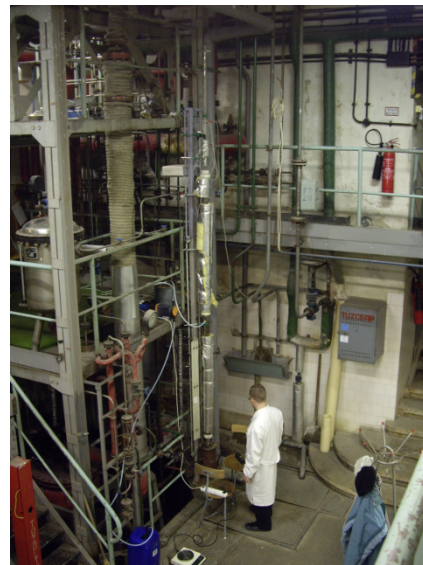
Swiss participant, **EPFL**

AOP process development,
combined chemical,
catalytic oxidation and
coupled biological
treatment

Coupled solar-biological
reactor at pilot scale



Pilot plant column
Sulzer structured
packing, 4 m high
 $N_{th} \sim 10 - 15$



Pilot scale oxidation
reactor GEOSAN Ltd
Pétfürdő



Hungarian participants

Jedlik project: **BME ABFS,**
CEPE, BSW, GEOSAN

complex treatment of
process wastewaters of
pharmaceutical production
HAS IOI high energy
radiation of wastewaters
containing organic
compounds, destruction of
dyes, drugs.

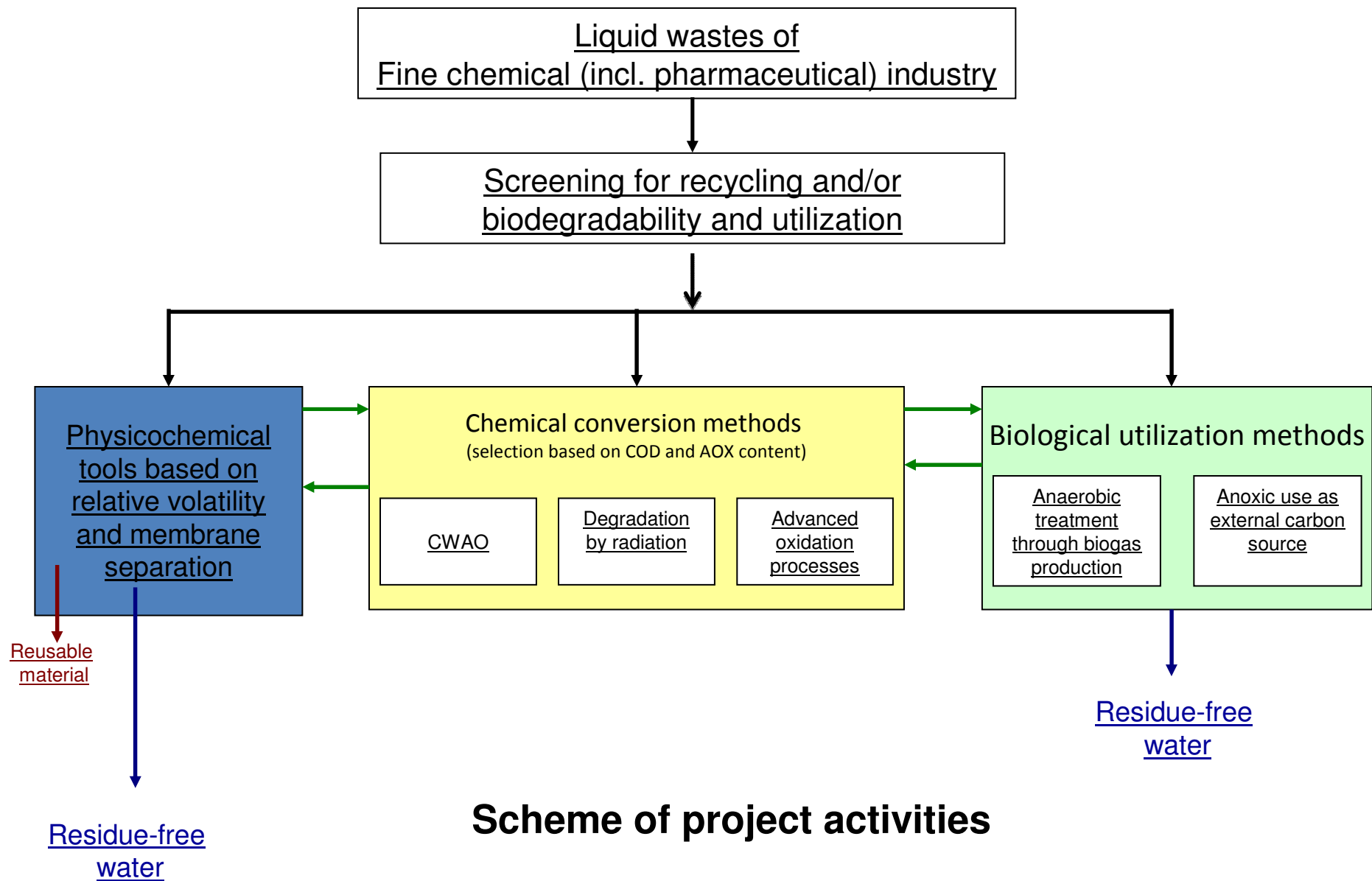
Starting points of the project

The pharmaceutical industry is leading in Switzerland and it is one of the main components of the chemical industry in Hungary.

Increasing production may well be accompanied by increased amounts of byproducts and wastes, among others carbon-rich, liquid wastes, disposed mainly through incineration.

The basic idea of the proposed project is, that major part of the carbon-rich wastes could be utilised in biological N-removal as carbon source for denitrification in domestic wastewater treatment, or for anaerobic biogas production.

The purpose of the project is (i) to elaborate a novel biological screening methodology taking the concentration dependence of biodegradability and toxicity as well as possibilities offered by the co-treatment with domestic wastewaters into consideration, (ii) to work out pretreatment procedures using physico-chemical separation processes, combined with chemical and/or catalytic methods in order to make originally non-biodegradable, toxic wastes utilisable and/or biodegradable, moreover remove residual bioactive compounds in treated water coming out from WWTP's.



Scheme of project activities

Primary elaborated selection method - respirometry

Test compounds used: **diclofenac, dimethyl formamide**

Investigated concentrations:

~300 mgCOD/l ~150 mgCOD/l

~75 mg COD/l

Minerals addition: **NH₄Cl, KH₂PO₄, K₂HPO₄, MgCl₂, CaCl₂**

Investigation of co-metabolism

co-substrate: **peptone**

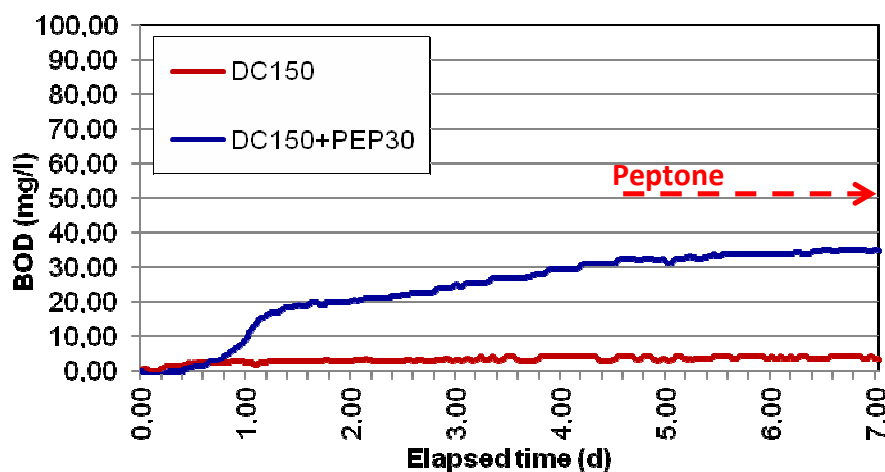
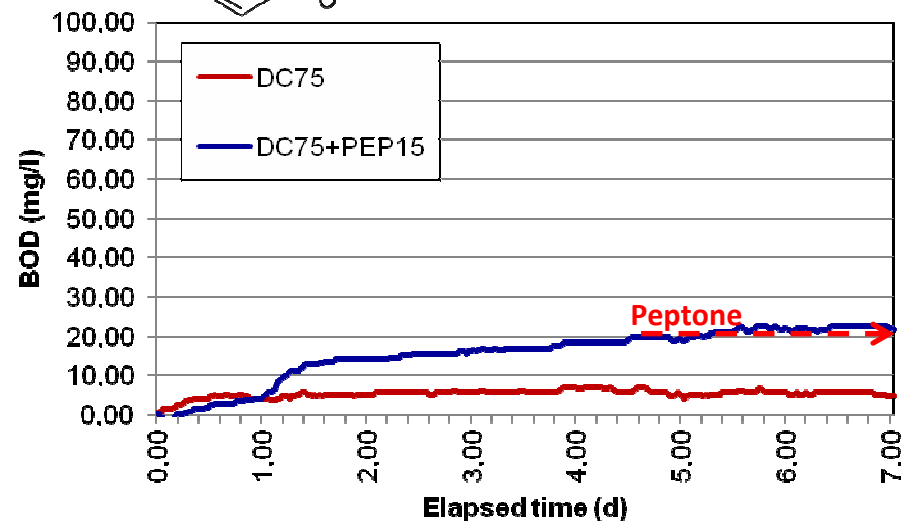
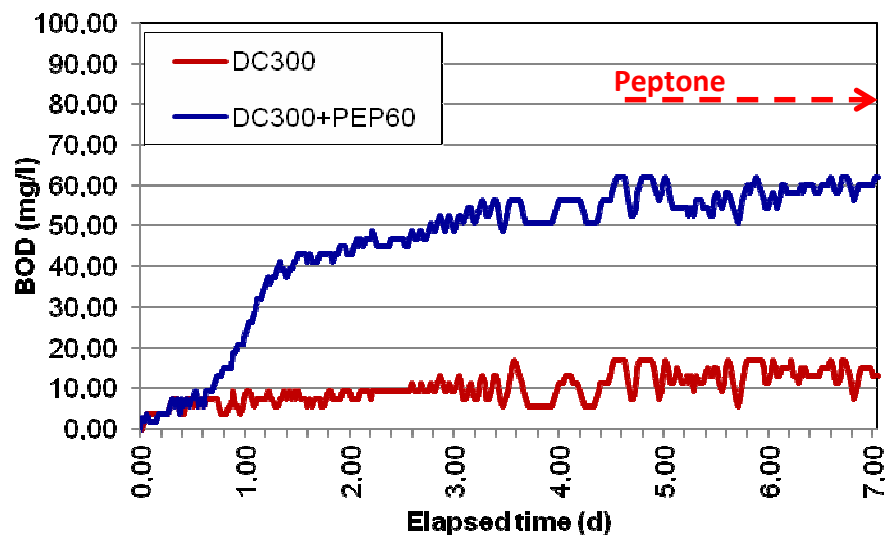
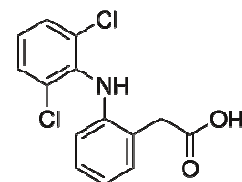
concentration: **20% of the test compound**

Origin of the seeding biomass: **domestic WWTP**

Temperature: **20 °C**, pH: **7,4-7,8**

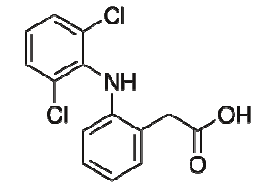
Real pharmaceutical wastewaters were also tested!

Test results for diclofenac

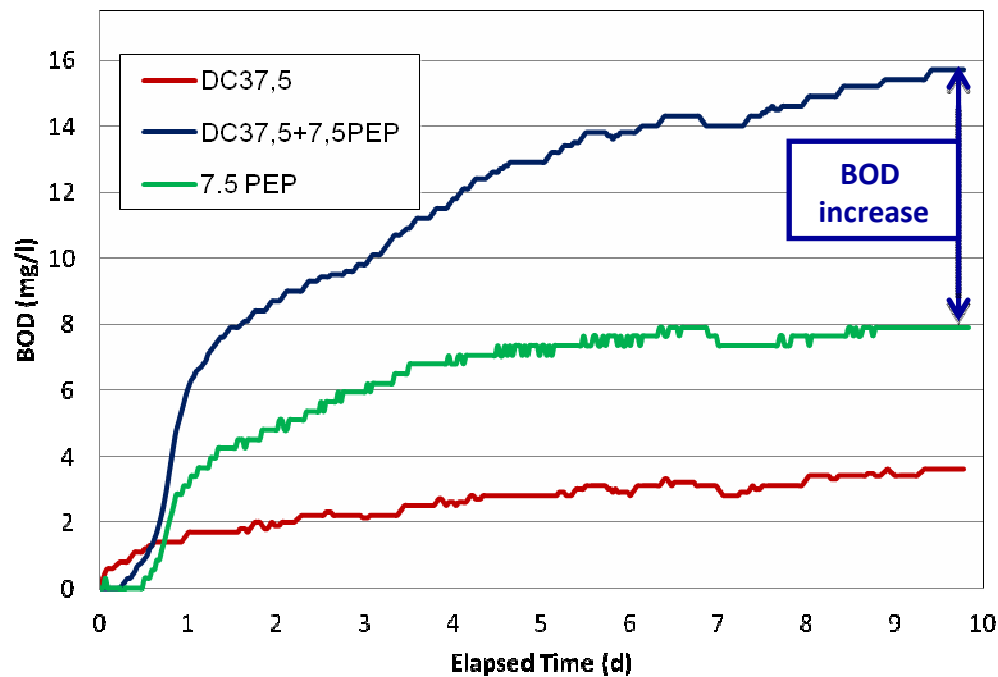


| BOD ₇ /COD ratio (%) | DC | DC + Peptone | Theor. peptone |
|---------------------------------|-----|--------------|----------------|
| Diclofenac conc. | | | |
| 283 mgCOD/l | 4,6 | 17,8 | 19,4 |
| 146 mgCOD/l | 2,2 | 20,3 | 23,9 |
| 83 mgCOD/l | 6,7 | 25,9 | 28,6 |

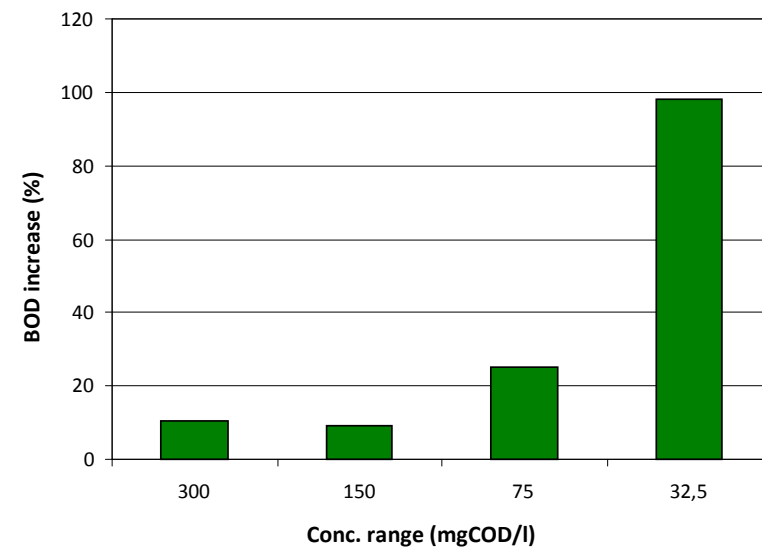
Diclofenac biodegradation with seeding biomass originated from domestic WWTP with 20 % industrial influent



DC 37.5



BOD increase with DC



Biodegradation of pharmaceutical real liquid wastes

Waste „B” – Total COD ~ 410 000 mg/l

Basic components:

Benzylamine HBr

Benzylamine HCl

Toluene

Dilution~1500x

| | BOD ₁₀ /COD (%) | COD removal (%) | Final COD (mg/l) |
|------------|----------------------------|-----------------|------------------|
| B300+PEP60 | 84 | 88 | 41 |
| B300 | 96 | 86 | 33 |

Biodegradation of pharmaceutical liquid wastes

Waste „II” – Total COD ~ 265 000 mg/l

Basic components: Sodium methyl sulphate, PEG, Methanol Dilution ~1000X

COD removal efficiency with peptone cofactor >80%

Biodegradation of pharmaceutical liquid wastes

Waste „XX” – Total COD ~ 455 000 mg/l

Basic components: Methanol, Morpholine Dilution~1000x

COD removal efficiency with peptone cofactor >60%

Determination of anaerobic biodegradability

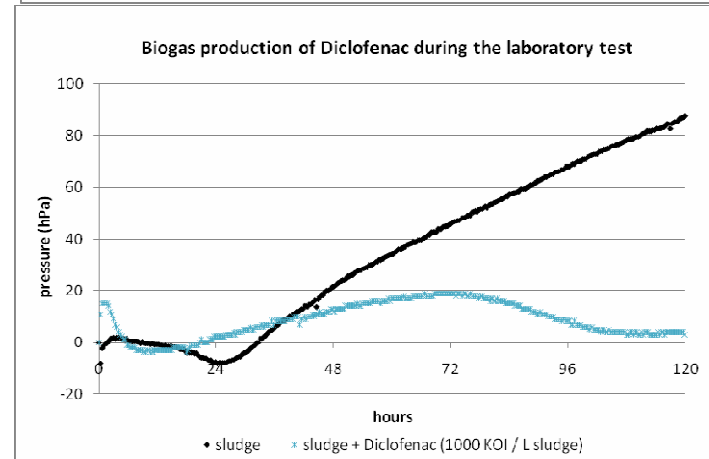
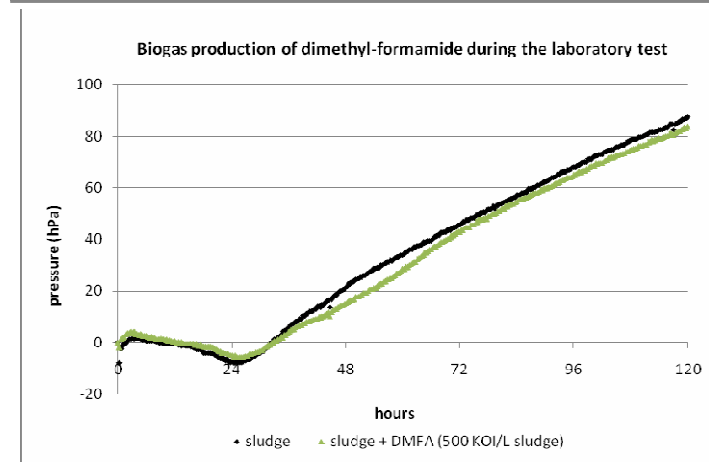
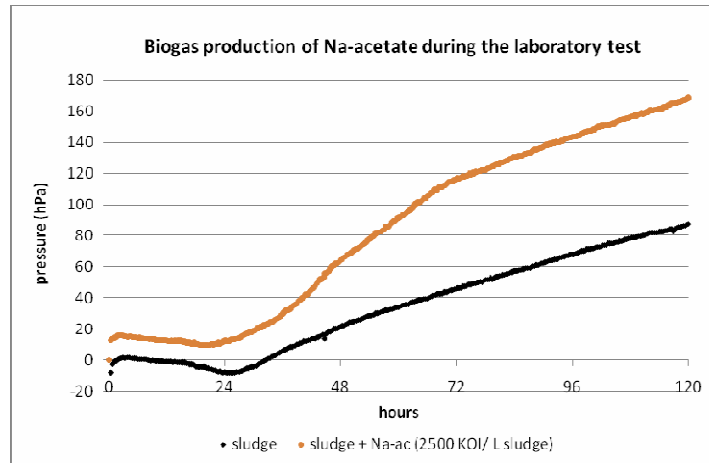


Anaerobic sludge spiked with sample and the blank are stirred at mesophile or thermophile temperature for 5-28 days.

The OXI-Top C heads measure the pressure differences in the bottles for calculating biogas production.

According to the biogas productions the anaerobic biodegradability of different samples can be compared.

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Biogas production

Anaerobic biodegradable
Model comp. Na acetate

Anaerobic non-biodegradable
DMF

Anaerobically toxic

EGIS wastewaters
are all anaerobic
non-biodegradable!!!

Conclusions of biodegradability tests

- **Elaboration of screening methods** for determining the biodegradability of liquid wastes and toxic materials has been **completed**.
- Selected methods: **respirometry, Zahn-Wellens test, anaerobic digestion test**
- Test compound diclofenac (DFC) has proved to be non-biodegradable and showed toxic effect on biomass adapted to domestic wastewater. With **WAO** application, residues of diclofenac were found to be readily **biodegradable**, already after 1 hour pretreatment time. **Biomass adapted to wastewater containing 20% industrial effluent could degrade DFC in small concentration.**
- Adaptation phase required for dimethylformamide biodegradation, could be significantly reduced both by peptone added as co-substrate and with WAO pretreatment.
- In **anaerobic digestion DMF** was not biodegradable, **DFC** was toxic as well. Pharmaceutical wastewaters were all **non degradable**.

Presence of VOC's in Process waste waters

- PWWs have special features, from fine chemical industry,
- In our project basically from pharmaceutical industry, organic pollutants, many of them volatile or forms heteroazeotrope with water
- The volatile organic pollutants can cause high Chemical Oxygen Demand (COD, **VOC-COD**), higher than 100,000 mg O₂/lit.
- Adsorbable Organic Halids (AOX) other problems, they usually form heteroazotrope with the water, or highly volatile e.g. dichlormethane
- AOX can be problematic at other treatment alternatives
- Emission limits: COD 1000 mg O₂/lit, AOX: 8 ppm

Comparison of rectification and stripping with air..

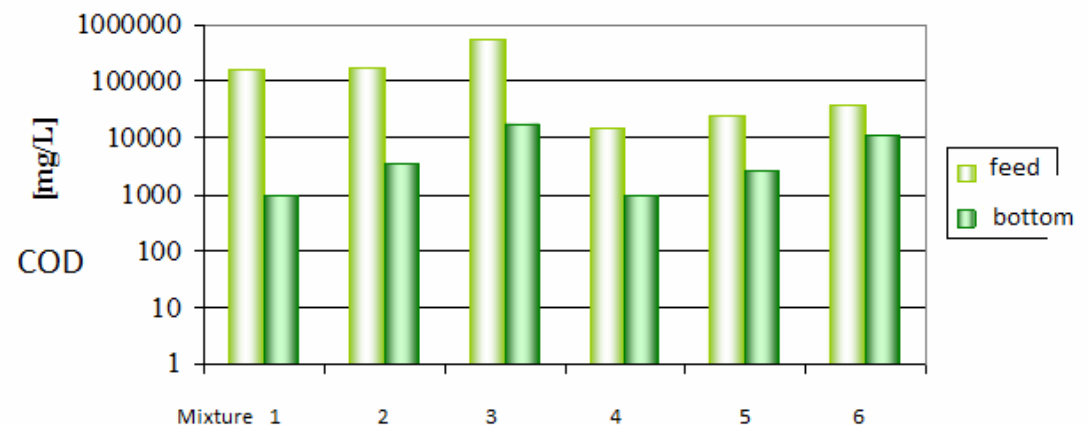
Removal of volatile pollutants (VOC-COD)

Removal of AOX

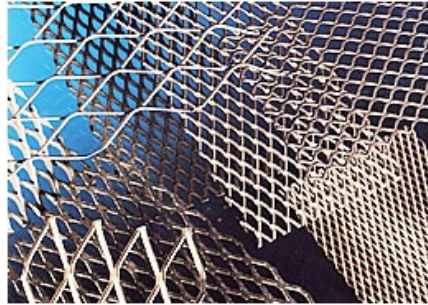
Design of AOX removing distillation (rectifying) column.

Membrane treatment

Non-VOC

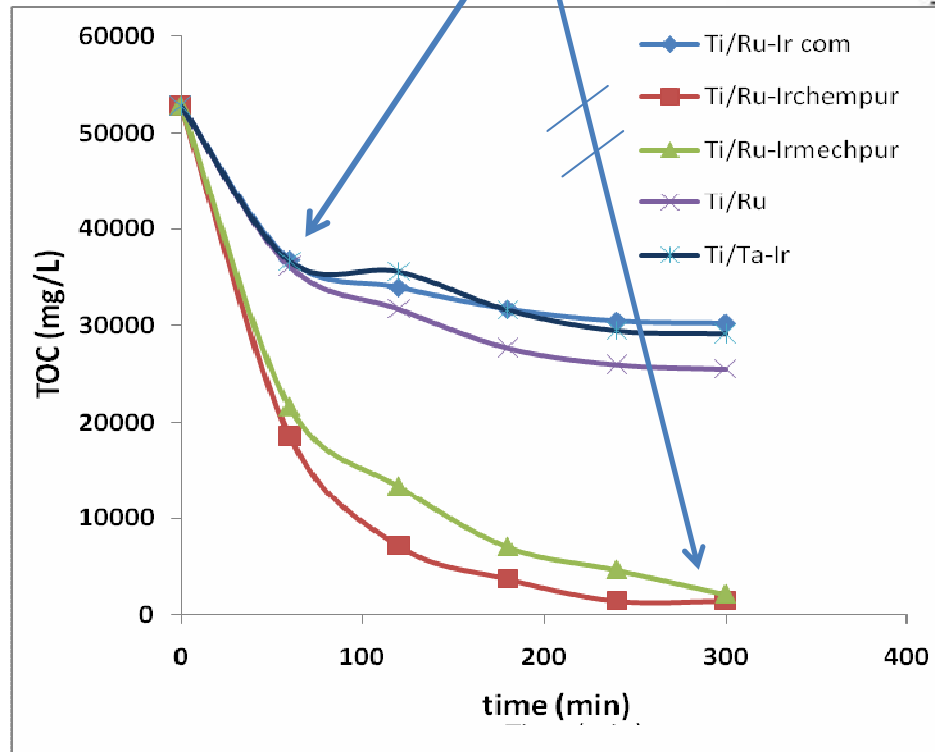
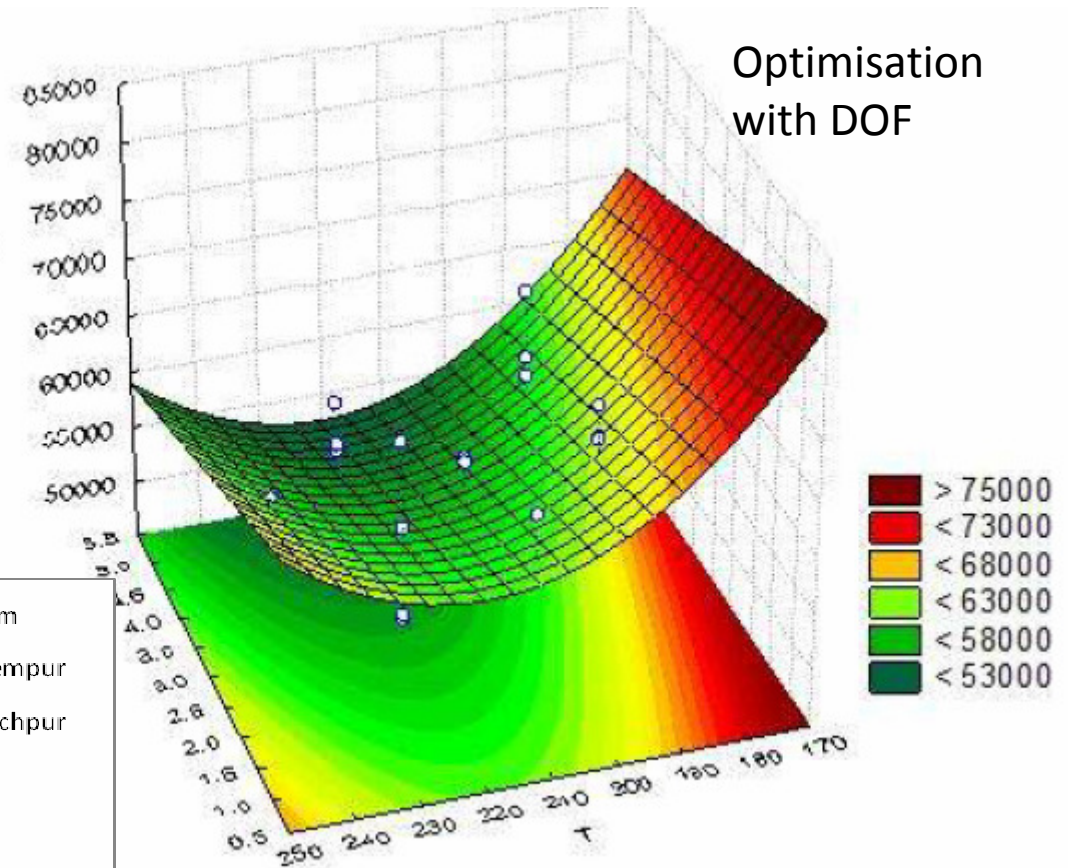


Wet oxidation of a process wastewater



No complete mineralization
!!!

COD



Catalytic wet oxidation at
temperatures above 200°C and
50 bar pressure

Analyzed treated wastewater from Lausanne WWTP:

| Family/Function | | Substances | LOQ (ng L ⁻¹) | Wastew. (ng L ⁻¹) |
|-----------------|----------------------------|------------------|------------------------------|----------------------------------|
| Pharmaceuticals | Lipid regulators | Bezafibrate | 8 | 426 |
| | | Gemfibrozil | 2 | 25 |
| | | Simvastatin | 15 | nd |
| | Antidiabetic drug | Metformin | 15 | 1,027 |
| | Antiepileptic drugs | Carbamazepine | 9 | 263 |
| | | Gabapentin | 7 | 1,737 |
| | Analgesics | Diclofenac | 15 | 518 |
| | | Ibuprofen | 15 | 112 |
| | | Ketoprofen | 10 | 123 |
| | | Mefenamic acid | 15 | 291 |
| | | Naproxen | 30 | 178 |
| | | Paracetamol | 50 | nd |
| | | Primidone | 5 | 49 |
| | Beta Blockers | Atenolol | 7 | 669 |
| | | Metoprolol | 5 | 179 |
| | | Sotalol | 5 | 260 |
| | Antibiotics | Azithromycin | 40 | 295 |
| | | Ciprofloxacin | 15 | 129 |
| | | Clarithromycin | 3 | 518 |
| | | Metronidazole | 50 | 456 |
| | | Norfloxacin | 15 | 27 |
| | | Ofloxacin | 15 | 41 |
| | | Sulfamethoxazole | 5 | 578 |
| | | Trimethoprim | 5 | 131 |

| Family/Function | | Substances | LOQ (ng L ⁻¹) | Wastew. (ng L ⁻¹) |
|-----------------------------|-----------------------------|---------------------|------------------------------|----------------------------------|
| Pharmaceuticals | X-Ray contrast media | Iohexol | | 10,920 |
| | | Iomeprol | | 4,268 |
| | | Iopamidol | 240 | 1,716 |
| | | Iopromide | 600 | nd |
| Corrosion Inhibitors | | Benzotriazole | 19 | 2,781 |
| | | Methylbenzotriazole | 10 | 1,535 |
| Biocides / Pesticides | Biocides | Triclosan | 50 | 135 |
| | Herbicides | Atrazin | 4 | 9 |
| | | Diuron | 40 | 57 |
| | | Isoproturon | 10 | nd |
| | | Mecoprop | 5 | 34 |
| | Algicides | Irgarol | 3 | nd |
| | | Terbutryn | 3 | 19 |

Treated wastewater:

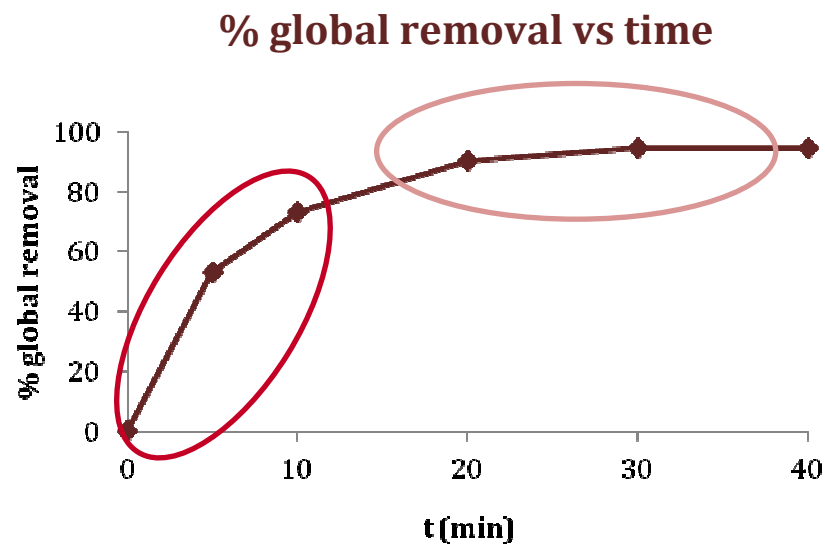
37 micropollutants were assessed at real concentrations (ng/L)

28 pharmaceuticals, 2 corrosion inhibitors and 7 biocides/pesticides

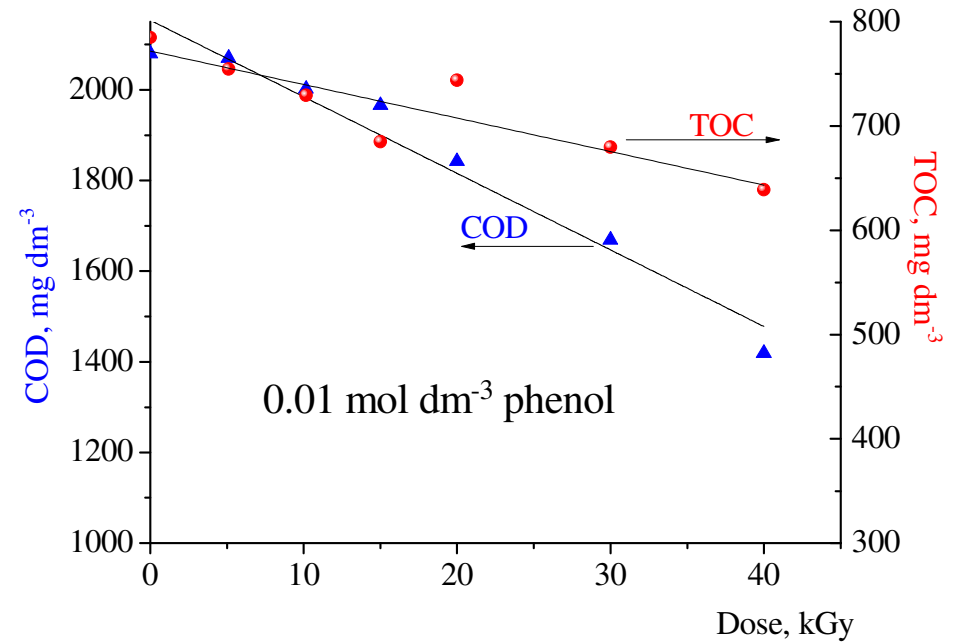
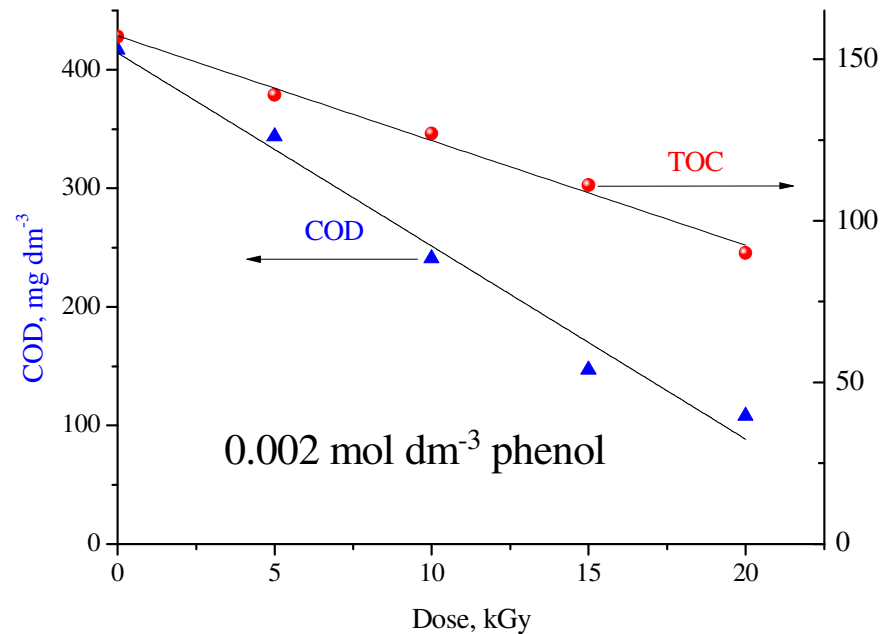
32 were found at the effluent of the WWTP → AOPs are required

Effect of the different versions of photo and photo-Fenton processes

| | UV | UV + H ₂ O ₂ (10 mg/L) | UV + H ₂ O ₂ (10 mg/L) + Fe (5mg/L) |
|------------------------------------|------|-------------------------------------------------|--------------------------------------------------------------|
| Pollutants degradation (30 min) | 80 % | 96 % | 95 % |



Irradiation (EB) combined with (catalytic) wet oxidation



Significant reduction of WO temperatures!

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Publications **EPFL**

Degradation of 32 emergent contaminants by uv and neutral photo-fenton in domestic wastewater effluent previously treated by activated sludge, N De la Cruz, J Giménez, S Esplugas, D Grandjean, L.F de Alencastro, C Pulgarín, Water research, in press

Emergent contaminants degradation by neutral photo-Fenton in domestic wastewater effluent previously treated by activated sludge. N. De la Cruz, J. Giménez, S. Esplugas, L.F. De Alencastro and C. Pulgarín. Mediterranean Congress of Chemical Engineering, Shaping the future of Chemical Engineering, Barcelona, Spain, November 15-18 2011,

High power impulse magnetron sputtering (HIPIMS) and traditional pulsed sputtering (DCMSP) Ag-surfaces leading to E. coli inactivation, O. Baghriche¹, A. P. Ehasarian², E. Kusiak-Nejman^{1,3}, C. Pulgarin¹, R. Sanjines⁴, A.W. Morawski³, J. Kiwi, Journal of Photochemistry and Photobiology A: Chemistry 227 (2012) 11– 17

Hungarian participants

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J. Tóth, F. Gergely, P. Mizsey: Physicochemical treatment of pharmaceutical wastewater: distillation and membrane processes, Periodica Polytechnica, 2011, 55/2, [IF: 0,042]

J. Tóth, P. Mizsey, Reduction of PWWs AOX, and COD values with physicochemical tools, http://www.hidrologia.hu/vandorgyules/29/dolgozatok/toth_andras_jozsef.html

Antal Tungler, Arezo M. Hosseini, Zoltán Schay, Sándor Szabó, János Kristóf, Éva Széles, Comparison of noble metal oxide/titanium monolith catalysts in wet oxidation of process wastewaters, Europacat X., Glasgow, 27 08 2011-02 09 2011

Chamam, M., Földváry, C.M., Hosseini, A.M., Tungler, A., Takács, E., Wojnárovits, L., Mineralization of aqueous phenolate solutions: a combination of irradiation treatment and wet oxidation. Radiation Physics and Chemistry accepted. doi: 10.1016/j.radphyschem.2011.11.013

Summary

- Project implementation according to schedule: project component 1 (characterization) completed
- Four scientific sessions with the Swiss partner up till now,, consensus in program planning, good complementarity
- Good results in biodegradation (project component 4, 5) , VOC removal (project component 2) , WO (project component 3) , AOP (project component 6)
- Pilot scale and industrial devices for distillation (operation at a pharma company), oxidation (project component 7), biodegradation (at Geosan) and biogas production (at BSW), coupled AOP and biodegradation (EPFL).



Thank you for your kind attention!